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### Thermodynamics of mixtures containing alkoxyethanols. Part xxiii. Speed of sound predictions and ultrasonic studies of hydroxyether + organic solvent mixtures

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## Thermodynamics of mixtures containing alkoxyethanols. Part xxiii. Speed of sound predictions and ultrasonic studies of hydroxyether + organic solvent mixtures

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The ability of different models to predict speeds of sound,  $u$ , of binary mixtures formed by alkoxyethanol and octane, oxaalkane or propylamine has been examined. The models applied are: the free length theory (LFT), the collision factor theory (CFT), and equations such as those proposed by Nomoto, Junjie or Van Dael. Collision factor theory, Nomoto's and Junjie's equations provide similar deviations between experimental and calculated  $u$ , which is represented quite accurately by these three models. Poorer predictions are obtained when applying the Junjie's equation to propylamine systems, probably due to the existence of strong interactions between unlike molecules in such mixtures. In contrast, slightly better  $u$  predictions from CFT are obtained for the systems 2-methoxyethanol + polyether, or hydroxyether + propylamine. The good  $u$  predictions obtained using Nomoto's equation remark the validity of Rao's assumption on additivity of molar sound velocity contributions from atoms, atom groups and chemical bonds of the constituent molecules. Discrepancies between experimental and calculated  $u$  are larger when using FLT than those obtained from CFT, Nomoto's or Junjie's equations. This has been ascribed to association and size or shape effects. The linear dependence on the molar fractions of the component liquids of the Rao's and Wada's constants suggests that there is no complex formation in the investigated mixtures, and that the interactions present in such systems are of dipolar type.

*Keywords:* Prediction; Speed of sound; Rao constant; Interactions; Hydroxyethers

### 1. Introduction

Alkoxyethanols are a very interesting class of substances, because the presence of the O and OH groups in the same molecule allows self-association via inter- and intramolecular hydrogen bonds. Different spectroscopic techniques have been used to investigate the existence of intramolecular hydrogen bonds [1–6], which are present at all conditions, even in vapour phase. In contrast, intermolecular H-bonds appear at

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higher concentrations of the hydroxyether in liquid state. For molecules of the type  $\text{CH}_3-(\text{CH}_2)_n-\text{O}-(\text{CH}_2)_p-\text{OH}$ , 5-, 6- and 7-membered rings are formed for  $p=2, 3$  and 4, respectively. Alkoxyethanols with two ether groups and  $n=1$  form 5-membered rings similar to those previously cited, but can also form 8-membered rings of quite different properties [4].

The formation of the intramolecular H-bonds leads to enhanced dipole-dipole interactions in solutions containing alkoxyethanols and alkanes relative to those present in mixtures with homomorphic alkanols [7]. Various evidence supports this conclusion. (a) The Trouton's constant of hydroxyethers,  $99.58 \text{ J mol}^{-1} \text{ K}^{-1}$ , is closer to the value of non-self-associated compounds,  $92.05 \text{ J mol}^{-1} \text{ K}^{-1}$ , than the value for 1-alkanols,  $110.88 \text{ J mol}^{-1} \text{ K}^{-1}$  [8]. (b) For a given alkane, the upper critical solution temperature (UCST) of the system including an alkoxyethanol is higher than that of the solution with the homomorphic 1-alkanol [7,9,10]. So,  $\text{UCST}(22\text{EEE} + n\text{-C}_7) = 286.98 \text{ K}$  [10], while 1-octanol is miscible with heptane at this temperature, as the molar excess enthalpies,  $H^E$ , values of this system indicate,  $366 \text{ J mol}^{-1}$  [11] at equimolar composition and at 288.15 K. (c)  $H^E$  (hydroxyether + alkane)  $>$   $H^E$  (homomorphic 1-alkanol + alkane) and the corresponding  $H^E$  curves for systems with alkoxyethanols are more symmetrical than those for alcoholic solutions, which are skewed towards low concentration of the self-associated compound. For example, at equimolar composition and 298.15 K,  $H^E$  (22BEE + heptane) =  $1008 \text{ J mol}^{-1}$  [12]  $>$   $H^E$  (1-decanol + heptane) =  $421 \text{ J mol}^{-1}$  [13]. All these features make the theoretical study of mixtures with alkoxyethanols very interesting. We have presented a complete treatment of hydroxyether + alkane systems [7] in terms of DISQUAC (*dispersive-quasichemical*) [14], a purely physical model based on the rigid lattice model developed by Guggenheim [15]. Then, we showed that the proximity effects between the O and OH groups of alkoxyethanols change substantially the interaction parameters of 1-alkanol +  $\text{CH}_3(\text{CH}_2)_u\text{O}(\text{CH}_2)_v\text{CH}_3$  mixtures [16]. We have also shown [17] that the thermodynamic properties of the mentioned solutions can be successfully represented using the so-called ERAS (*extended real associated solution*) model [18], which combines the real association solution model [19] with Flory's equation of state [20]. Moreover, both models, DISQUAC and ERAS, have been used to study mixtures of hydroxyethers with linear monoalkanes or 1-alkanols [21]. In addition, orientational effects in this kind of systems have been examined using the Flory theory [22]. We have also reported experimental data on density,  $\rho$ ,  $u$  and on related quantities such as molar excess volumes,  $V^E$ , or isothermal and isentropic compressibilities for alkoxyethanol + dibutylether mixtures [23,24]. As continuation, we present here a detailed comparison between  $u$  predictions for binary mixtures formed by hydroxyether and organic solvent (octane, oxaalkanes or propylamine) from the FLT [25,26], CFT [27] and from equations such as Nomoto [28], Junjie [29] or Van Dael [30]. This is important from a practical point of view, as oxygenated compounds are increasingly used as additives to gasoline due their octane-enhancing and pollution-reducing properties [31,32]. In addition, hydroxyethers are non-ionic amphiphile molecules, very effective as surfactants with a large number of applications [33–36]. Finally, in order to gain a deeper insight into the interactions present in alkoxyethanol systems, we investigate such interactions in terms of the the molar sound velocities  $R_i$  [37], Wada's constant [38] or the so-called molecular interaction parameter [39].

## 2. Theories

### 2.1. Free length theory (FLT) [25,26]

Intermolecular free length is defined as [40]:

$$L_f = \frac{2V_a}{Y} \quad (1)$$

where  $V_a$  is the available volume and  $Y$  is the surface area per mole. These quantities are calculated for pure liquids as follows:

$$V_a = V - V_0 \quad (2)$$

$$Y = (36\pi N_A V_0^2)^{1/3} \quad (3)$$

$V$  is the molar volume,  $V_0 = V(1 - T/T_C)^{0.3}$ , the molar volume at 0 K and  $N_A$  the Avogadro's number.  $T_C$  stands for the critical temperature. In the case of a binary mixture,  $L_f$  is generalized:

$$L_f = \frac{2[V - \sum x_i V_{0i}]}{\sum x_i Y_i} \quad (4)$$

The value of  $L_f$  so obtained is known as thermodynamic  $L_f$ . Speeds of sound can be evaluated from the empirical equation obtained by Jacobson [26]:

$$L_f = K k_s^{1/2} \quad (5)$$

where  $K$  is a constant dependent on the temperature and  $k_s$  is the isentropic compressibility of the mixture. Taking into account the Laplace equation,  $k_s = 1/\rho u^2$

$$u = \frac{K}{L_f \rho^{1/2}} \quad (6)$$

### 2.2. Collision factor theory (CFT) [27]

In this theory, the available volume for a pure liquid is determined from the expression:

$$V_a = V - SB \quad (7)$$

where  $S$  is the collision factor and  $B$  is the actual volume of the molecules per mole, which is calculated as

$$B = \frac{4}{3} \pi N_A r^3 \quad (8)$$

with the molecular radius determined by the Schaaffs relation:

$$r = \sqrt[3]{\frac{M}{\rho N_A}} \sqrt[3]{\frac{3}{16\pi} \left[ 1 - \frac{\gamma RT}{Mu^2} \left( \sqrt{1 + \frac{Mu^2}{3\gamma RT}} - 1 \right) \right]} \quad (9)$$

Here,  $M$  is the molecular weight and  $\gamma$  the ratio of heat capacities,  $C_p/C_v$ . It has been shown that this equation is a reliable method to estimate the molecular radius of liquids [41]. The collision factor is estimated from the expression:

$$S = \frac{uV}{1600B} \quad (10)$$

Equations (9) and (10) are obtained starting from the van der Waals equation. The latter is generalized to predict  $u$  of liquid mixtures:

$$u = 1600 \frac{(\sum x_i S_i)(\sum x_i B_i)}{V} \quad (11)$$

It is possible to combine equations (2) and (10) and calculate  $u$  as

$$u = \frac{1600V_0}{V} \quad (12)$$

### 2.3. Nomoto's equation [28]

Nomoto [28], under the assumptions that the molar sound velocities are additive and that there is no volume change on mixing, derived the following expression:

$$u = \left[ \frac{x_1 R_1 + x_2 R_2}{x_1 V_1 + x_2 V_2} \right]^{1/3} \quad (13)$$

where  $V_i$  is the molar volume of component  $i$  and  $R_i$  a quantity characteristic of each compound, which was found experimentally independent of the temperature [38].  $R_i$  is called Rao's constant or molar sound velocity, and is defined by:

$$R_i = V_i u_i^{1/3} \quad (14)$$

It is remarkable that  $R_i$  is additive, i.e., it can be calculated as a sum of increments from the atoms or atoms groups in the molecule, and from chemical bonds. Another quantity of similar nature of  $R_i$  was introduced by Wada under the name of molecular compressibility [38],  $W_i$ , defined as:

$$W_i = V_i \kappa_{si}^{-1/7} \quad (15)$$

### 2.4. Junjie's and Van Dael's equations

These equations have widely used to provide predictions on  $u$  of liquid mixtures. They are based on the ideal mixture concept, assuming that  $\kappa_S^{id} = \phi_1 \kappa_{S1} + \phi_2 \kappa_{S2}$  ( $\phi_i$  is the volume fraction), which directly leads to the Junjie's equation [29]:

$$u = \frac{x_1 V_1 + x_2 V_2}{(x_1 M_1 + x_2 M_2)^{1/2}} \left[ \frac{x_1 V_1^2}{M_1 u_1^2} + \frac{x_2 V_2^2}{M_2 u_2^2} \right]^{-1/2} \quad (16)$$

Table 1. Source of excess molar volumes,  $V^E$ , speed of sounds,  $u$ , and isentropic compressibilities,  $\kappa_s$ , used in this work for hydroxyether + organic solvent mixtures at temperature  $T$ .

System	$T(K)$	$V^E(\text{cm}^3 \text{mol}^{-1})$	Ref. $u, \kappa_s$
2-Ethoxyethanol (2EE) + <i>n</i> -octane	298.15	0.753 [64]	[64]
2-Propoxyethanol (2PE) + <i>n</i> -octane	298.15	0.588 [64]	[64]
2-Isopropoxyethanol (2IPE) + <i>n</i> -octane	298.15	0.774 [64]	[64]
2-Butoxyethanol (2BE) + <i>n</i> -octane	298.15	0.444 [64]	[64]
2-Isobutoxyethanol (2IBE) + <i>n</i> -octane	298.15	0.566 [64]	[64]
2-Methoxyethanol (2ME) + dibutylether (4O4)	298.15	0.312 [23]	[23]
2-Ethoxyethanol + dibutylether	298.15	0.226 [23]	[23]
2-Butoxyethanol + dibutylether	298.15	-0.054 [23]	[23]
2-Methoxyethanol + dibutylether	303.15	0.332 [23]	[23]
2-Ethoxyethanol + dibutylether	303.15	0.247 [23]	[23]
2-Butoxyethanol + dibutylether	303.15	-0.044 [23]	[23]
2-(2-Methoxyethoxy)ethanol (22ME) + dibutylether	298.15	0.158 [24]	[24]
2-(2-Ethoxyethoxy)ethanol (22EE) + dibutylether	298.15	0.142 [24]	[24]
2-(2-Butoxyethoxy)ethanol (22BE) + dibutylether	298.15	-0.1057 [24]	[24]
2-(2-Methoxyethoxy)ethanol + dibutylether	303.15	0.166 [24]	[24]
2-(2-Ethoxyethoxy)ethanol + dibutylether	303.15	0.153 [24]	[24]
2-(2-Butoxyethoxy)ethanol + dibutylether	303.15	-0.103 [24]	[24]
2-{2-(2-Methoxyethoxy)ethoxy}ethanol (222MEEE) + dibutylether	298.15	0.0887 [65]	[66]
2-{2-(2-Ethoxyethoxy)ethoxy}ethanol (222EEEE) + dibutylether	298.15	0.0981 [65]	[66]
2-{2-(2-Butoxyethoxy)ethoxy}ethanol (222BEEE) + dibutylether	298.15	-0.1254 [65]	[66]
2-Methoxyethanol + 2,5-dioxahexane (1O2O1)	298.15	-0.2242 [67]	[68]
2-Methoxyethanol + 2,5,8-trioxanonane (1O2O2O1)	298.15	-0.0944 [67]	[68]
2-Methoxyethanol + 2,5,8,11-tetraoxadodecane (1O2OO2O1)	298.15	-0.0943 [68]	[68]
2-Methoxyethanol + 3,6,9-trioxaundecane (2O2O2O2)	298.15	-0.1867 [67]	[68]
2-Methoxyethanol + 5,8,11-trioxapentadecane (4O2O2O4)	298.15	0.0854 [67]	[68]
2-Methoxyethanol + propylamine	298.15	-1.2214 [69]	[70]
2-(2-Methoxyethoxy)ethanol + propylamine	298.15	-1.3131 [69]	[70]
2-(2-Ethoxyethoxy)ethanol + propylamine	298.15	-1.5984 [69]	[70]
2-(2-Butoxyethoxy)ethanol + propylamine	298.15	-1.4169 [69]	[70]
2-{2-(2-Methoxyethoxy)ethoxy}ethanol + propylamine	298.15	-1.4559 [69]	[70]

The Van Dael's equation is derived taking into account that  $V_1 = V_2$  [30]:

$$\frac{1}{u^2} = \left( \frac{x_1}{M_1 u_1^2} + \frac{x_2}{M_2 u_2^2} \right) (x_1 M_1 + x_2 M_2) \quad (17)$$

### 3. Results

Table 1 lists the source of the experimental data on  $V^E$ ,  $u$  and  $k_s$  for the systems studied. The physical constants of pure compounds needed to obtain  $u$  predictions from the different theories applied in this work are collected in table 2. In the case of FLT, calculations were developed assuming constant values of  $K$  (equation (5)) along each homologous series. The values used are collected in table 3.  $K$  values dependent on the concentration ( $K = x_1 K_1 + x_2 K_2$ ) have been considered in the literature [42,43]. Table 4 shows a comparison between the  $u$  predictions obtained from the different models considered. This table records relative standard deviations for  $u$  defined as

$$\sigma_r(u) = \left\{ \frac{1}{N} \sum \left[ \frac{u_{\text{exp}} - u_{\text{calc}}}{u_{\text{exp}}} \right]^2 \right\}^{1/2} \quad (18)$$

Table 2. Physical constants of pure compounds at 298.15 K: molar volume,  $V$ , isentropic compressibility,  $\kappa_s$ , molar heats capacity at constant pressure,  $C_p$  and constant volume,  $C_v$ , speed of sound,  $u$  and critical temperature,  $T_C$ .

Compound <sup>a</sup>	$V(\text{cm}^3 \text{mol}^{-1})$	$\alpha(10^{-4} \text{K}^{-1})$	$\kappa_s(\text{TPa}^{-1})$	$C_p(\text{J mol}^{-1} \text{K}^{-1})$	$C_v(\text{J mol}^{-1} \text{K}^{-1})$	$u(\text{m s}^{-1})$	$T_C(\text{K})$
2ME	79.26 <sup>b</sup> 79.64 <sup>b,d</sup>	9.560 <sup>b</sup>	578.77 <sup>b</sup>	172.43 <sup>b</sup> 172.43 <sup>b,e</sup>	141.75 <sup>b</sup> 141.75 <sup>b,e</sup>	1341.5 <sup>b</sup> 1324.2 <sup>b,d</sup>	597.6 <sup>c</sup> 597.6 <sup>c</sup>
2EE	97.43 <sup>b</sup> 97.91 <sup>b,d</sup>	9.833 <sup>b</sup>	636.96 <sup>b</sup>	207.21 <sup>b</sup> 207.21 <sup>b,e</sup>	170.90 <sup>b</sup> 170.90 <sup>b,e</sup>	1301.7 <sup>b</sup> 1284.1 <sup>b,d</sup>	586.3 <sup>f</sup> 586.3 <sup>e</sup>
2PE	114.76 <sup>g</sup>	10.03 <sup>g</sup>	652.40 <sup>g</sup>	246.53 <sup>g</sup>	203.1 <sup>g</sup>	1299.6 <sup>g</sup>	615.2 <sup>h</sup>
2IPE	115.32 <sup>g</sup>	11.20 <sup>g</sup>	691.18 <sup>g</sup>	239.56 <sup>g</sup>	189.9 <sup>g</sup>	1267.9 <sup>g</sup>	593.2 <sup>f</sup>
2BE	131.90 <sup>b</sup> 132.52 <sup>b,d</sup>	9.346 <sup>b</sup>	655.33 <sup>b</sup>	268.9 <sup>b</sup> 268.9 <sup>b,e</sup>	225.1 <sup>b</sup> 225.1 <sup>b,e</sup>	1305.0 <sup>b</sup> 1288.1 <sup>b,d</sup>	633.9 <sup>h</sup> 633.9 <sup>e</sup>
2IBE	133.33 <sup>g</sup>	9.44 <sup>g</sup>	710.72 <sup>g</sup>	278.6 <sup>g</sup>	235.3 <sup>g</sup>	1259.9 <sup>g</sup>	615 <sup>f</sup>
22MEE	118.32 <sup>i</sup> 118.85 <sup>i,d</sup>	8.493 <sup>i</sup>	491.72 <sup>i</sup>	262.1 <sup>i</sup> 262.1 <sup>e</sup>	216.6 <sup>i</sup> 216.6 <sup>e</sup>	1415.2 <sup>i</sup> 1397.9 <sup>i,d</sup>	672 <sup>c</sup> 672 <sup>c</sup>
22EEE	136.45 <sup>i</sup> 137.08 <sup>i,d</sup>	9.242 <sup>i</sup>	538.40 <sup>i</sup>	297.2 <sup>i</sup> 297.2 <sup>e</sup>	244.2 <sup>i</sup> 244.2 <sup>e</sup>	1374.3 <sup>i</sup> 1356.6 <sup>i,d</sup>	670 <sup>c</sup> 670 <sup>c</sup>
22BEE	171.11 <sup>i</sup> 171.90 <sup>i,d</sup>	8.918 <sup>i</sup>	572.80 <sup>i</sup>	354.9 <sup>i</sup> 354.9 <sup>e</sup>	295.8 <sup>i</sup> 295.8 <sup>e</sup>	1356.9 <sup>i</sup> 1339.9 <sup>i,d</sup>	692.3 <sup>h</sup> 692.3 <sup>e</sup>
222MEEE	157.43 <sup>j</sup>	8.28 <sup>j</sup>	450.5 <sup>j</sup>	358 <sup>j</sup>	298.5 <sup>j</sup>	1458.9 <sup>j</sup>	679.6 <sup>f</sup>
222EEEE	175.40 <sup>j</sup>	8.55 <sup>j</sup>	490 <sup>j</sup>	389 <sup>j</sup>	324 <sup>j</sup>	1417.3 <sup>j</sup>	701.9 <sup>f</sup>
222BEEE	209.03 <sup>j</sup>	8.53 <sup>j</sup>	517.9 <sup>j</sup>	450 <sup>j</sup>	376.7 <sup>j</sup>	1398.8 <sup>j</sup>	747 <sup>f</sup>
Octane	160.69 <sup>g</sup>	11.64 <sup>g</sup>	1040.16 <sup>g</sup>	254.2 <sup>g</sup>	207.3 <sup>g</sup>	1173.4 <sup>g</sup>	568.8 <sup>k</sup>
4O4	170.41 <sup>b</sup> 171.43 <sup>b,d</sup>	11.336 <sup>b</sup>	971.12 <sup>b</sup>	278 <sup>b</sup> 278 <sup>e</sup>	224 <sup>b</sup> 224 <sup>e</sup>	1160.9 <sup>b</sup> 1141.8 <sup>b,d</sup>	588.1 <sup>k</sup> 588.1 <sup>e</sup>
1O2O1	104.47 <sup>l</sup>	12.8 <sup>l</sup>	854.1 <sup>l</sup>	193.3 <sup>l</sup>	147.7 <sup>l</sup>	1165.1 <sup>l</sup>	537
1O2O2O1	142.90 <sup>l</sup>	10.6 <sup>l</sup>	651.5 <sup>l</sup>	279.6 <sup>l</sup>	221.5 <sup>l</sup>	1278.6 <sup>l</sup>	569.7 <sup>f</sup>
1O2O2O2O1	181.74 <sup>l</sup>	9.7 <sup>l</sup>	567.11	367.6 <sup>l</sup>	294.5 <sup>l</sup>	1340.9 <sup>l</sup>	636.4 <sup>f</sup>
2O2O2O2	179.56 <sup>l</sup>	11.1 <sup>l</sup>	720 <sup>l</sup>	347.4 <sup>l</sup>	274.9 <sup>l</sup>	1239.8 <sup>l</sup>	614 <sup>f</sup>
4O2O2O4	248.64 <sup>l</sup>	12.7 <sup>l</sup>	707 <sup>l</sup>	479.6 <sup>l</sup>	354.6 <sup>l</sup>	1269 <sup>l</sup>	702.3 <sup>f</sup>
propylamine	82.99 <sup>m</sup>	13.78 <sup>m</sup>	950.8 <sup>m</sup>	161 <sup>m</sup>	123.2 <sup>m</sup>	1215.2 <sup>m</sup>	497 <sup>n</sup>

<sup>a</sup>For symbols, see table 1; <sup>b</sup>[23]; <sup>c</sup>[71]; <sup>d</sup>value at 303.15 K; <sup>e</sup>value used at 303.15 K; <sup>f</sup>calculated using the Joback's method [72]; <sup>g</sup>[64]; <sup>h</sup>[73]; <sup>i</sup>[24]; <sup>j</sup>[66]; <sup>k</sup>[74]; <sup>l</sup>[68]; <sup>m</sup>[70]; <sup>n</sup>[75].

 Table 3. Values of Jacobson's constant (equation (5)) at temperature  $T$  used in this work.

System	$T(\text{K})$	$K(\text{kg}^{1/2} \text{m}^{1/2} \text{s}^{-1})$
2-Alkoxyethanol + octane	298.15	$1.92 \times 10^{-6}$
2-Alkoxyethanol + dibutylether	298.15	$1.92 \times 10^{-6}$
	303.15	$1.96 \times 10^{-6}$
2-(2-Alkoxyethoxy)ethanol + dibutylether	298.15	$1.92 \times 10^{-6}$
	303.15	$1.96 \times 10^{-6}$
2-{2-(2-Alkoxyethoxy)ethoxy}ethanol + dibutylether	298.15	$2 \times 10^{-6}$
2-Methoxyethanol + polyoxaalkane	298.15	$2.1 \times 10^{-6}$
Hydroxyether + propylamine	298.15	$2 \times 10^{-6}$

For the sake of clarity, a summary of results is shown in table 5. Table 6 contains values of the interaction molecular parameter,  $X$  [44,45] and of  $\Delta L_f$  defined, respectively, as

$$\chi = \left( \frac{u_{\text{exp}}}{u_{\text{id}}} \right)^2 - 1 \quad (19)$$

$$\Delta L_f = L_f - \phi_1 L_{f1} + \phi_2 L_{f2} \quad (20)$$

being  $L_f$  calculated accordingly to equation (4) (thermodynamic intermolecular free length).

Table 4. Speeds of sound at equimolar composition and temperature  $T$  for hydroxyether + organic solvent mixtures. Comparison of experimental (exp.) results with those provided by equations applied in this work. Also included are the relative standard deviations defined by equation (18).

System <sup>a</sup>	$T(K)$	$u(m s^{-1})$ exp. <sup>b</sup>	$u(m s^{-1})$ FLT	$u(m s^{-1})$ equation (12)	$u(m s^{-1})$ CFT	$u(m s^{-1})$ Nomoto	$u(m s^{-1})$ Junjie	$u(m s^{-1})$ Van Dael
2EE + <i>n</i> -C <sub>8</sub>	298.15	1186.3	1177.4 0.012	1277.4 0.071	1214.7 0.018	1220.8 0.022	1198.4 0.008	1232.2 0.029
2PE + <i>n</i> -C <sub>8</sub>	298.15	1197.9	1199.1 0.002	1287.9 0.071	1221 0.014	1224.9 0.017	1203.7 0.004	1233.1 0.021
2IPE + <i>n</i> -C <sub>8</sub>	298.15	1183.6	1166.7 0.016	1280.4 0.076	1206.1 0.014	1212.2 0.018	1194.4 0.007	1218.8 0.022
2BE + <i>n</i> -C <sub>8</sub>	298.15	1208.9	1209.4 0.001	1295.4 0.069	1292.2 0.012	1231.6 0.014	1210.5 0.002	1231.8 0.014
2IBE + <i>n</i> -C <sub>8</sub>	298.15	1189.7	1184.1 0.005	1289.5 0.079	1208.1 0.011	1212 0.014	1196.9 0.005	1212.7 0.014
2ME + 4O4	298.15	1194.1	1215.3 0.018	1292.9 0.081	1214.1 0.013	1216.4 0.014	1195.7 0.001	1221.2 0.018
2EE + 4O4	298.15	1195.8	1191.5 0.016	1291.5 0.079	1209.7 0.009	1210.9 0.000	1195.9 0.0006	1217.6 0.013
2BE + 4O4	298.15	1215.9	1222.7 0.004	1306.9 0.077	1224.4 0.005	1222.4 0.004	1208.6 0.005	1228.7 0.007
22MEE + 4O4	298.15	1233.6	1233.2 0.008	1312.3 0.072	1264.2 0.017	1261.2 0.016	1220.2 0.009	1273.4 0.023
22EEE + 4O4	298.15	1232.3	1221.8 0.014	1313.7 0.072	1254.7 0.013	1252.9 0.012	1220.9 0.007	1252.5 0.012
22BEE + 4O4	298.15	1245.5	1231.5 0.015	1323.6 0.070	1259.3 0.008	1252.6 0.006	1230.3 0.009	1229.7 0.009
222MEEE + 4O4	298.15	1265.5	1304.5 0.052	1318.1 0.068	1302.6 0.021	1298.4 0.019	1242.9 0.014	1260.1 0.004
222EEEE + 4O4	298.15	1263.6	1319.4 0.053	1324.5 0.066	1289.1 0.014	1286.7 0.013	1241.9 0.013	1235.9 0.017
222BEEE + 4O4	298.15	1273.4	1359.2 0.070	1338.6 0.065	1290.6 0.010	1288.3 0.008	1250.3 0.013	1205.9 0.039
2ME + 4O4	303.15	1175.6	1210.4 0.029	1286.1 0.091	1195.5 0.013	1197.7 0.014	1176.8 0.001	1203.6 0.019
2EE + 4O4	303.15	1177.2	1186.5 0.010	1284.6 0.089	1191 0.009	1192.3 0.009	1177.1 0.0008	1199.4 0.014
2BE + 4O4	303.15	1197.8	1218.2 0.015	1300.4 0.087	1206.1 0.005	1204.1 0.004	1189.9 0.005	1210.5 0.007
22MEE + 4O4	303.15	1215.5	1229.2 0.010	1306 0.081	1245.7 0.017	1242.5 0.015	1201.2 0.010	1254.6 0.023
22EEE + 4O4	303.15	1214.4	1217.7 0.009	1307.5 0.081	1236.2 0.013	1234.2 0.012	1201.9 0.008	1233.7 0.011
22BEE + 4O4	303.15	1227.8	1227.9 0.009	1317.6 0.079	1241.1 0.008	1238.4 0.006	1211.6 0.009	1211.2 0.010
2ME + 1O2O1	298.15	1244.1	1346.9 0.085	1277.6 0.041	1244.5 0.0003	1239.5 0.003	1226.1 0.011	1247 0.001
2ME + 1O2O2O1	298.15	1304.4	1280.4 0.064	1289.4 0.016	1300.3 0.003	1300.8 0.002	1299.6 0.003	1266.4 0.021
2ME + 1O2O2O2O1	298.15	1345	1322.7 0.058	1317.6 0.022	1337. 0.005	1341.1 0.003	1341 0.003	1228.4 0.063
2ME + 2O2O2O2	298.15	1272.7	1322.1 0.059	1309.5 0.034	1269.7 0.003	1270.4 0.002	1266.7 0.004	1218.1 0.031
2ME + 4O2O2O4	298.15	1280.1	1390.4 0.090	1341.6 0.047	1279.6 0.001	1286.3 0.004	1283.4 0.002	1157.2 0.070
2ME + propylamine	298.15	1296.4	1385.6 0.058	1276.2 0.018	1296.2 0.001	1275.8 0.010	1249.2 0.025	1255.8 0.021
22MEE + propylamine	298.15	1347.3	1392 0.028	1306.8 0.032	1345.8 0.003	1330.3 0.008	1284.2 0.032	1195.6 0.081
22EE + propylamine	298.15	1330	1385.8 0.031	1312.6 0.015	1327.9 0.003	1312.6 0.008	1278.7 0.027	1159.2 0.093
22BE + propylamine	298.15	1328	1317.6 0.012	1316.9 0.006	1314.2 0.007	1302.1 0.013	1241.1 0.047	1104.9 0.122
222MEE + propylamine	298.15	1389.8	1323.8 0.052	1316.6 0.046	1382.1 0.010	1371.4 0.005	1314.4 0.028	1118.5 0.134

<sup>a</sup>For symbols, see table 1;

<sup>b</sup>for the source of data, see table 1.



Table 5. Mean standard relative deviations<sup>a</sup> for  $u$  of hydroxyether + organic solvent mixtures obtained in this work from the different models applied.

System <sup>b</sup>	FLT	Equation (12)	CFT	Nomoto	Junjie	Van Dael
2-Alkoxyethanol + octane <sup>c</sup>	0.0072	0.0732	0.0138	0.017	0.0048	0.020
2-Alkoxyethanol + 4O4 <sup>c</sup>	0.0127	0.0522	0.009	0.009	0.0022	0.010
2-(2-Alkoxyethoxyethanol) + 4O4 <sup>c</sup>	0.0123	0.0713	0.0127	0.0113	0.0083	0.0147
2-{2-(2-Alkoxyethoxy)ethoxy}ethanol + 4O4 <sup>c</sup>	0.0583	0.066	0.015	0.0133	0.0133	0.020
2-Alkoxyethanol + 4O4 <sup>d</sup>	0.0180	0.089	0.009	0.009	0.0023	0.0133
2-(2-Alkoxyethoxyethanol) + 4O4 <sup>d</sup>	0.0093	0.0803	0.0127	0.0103	0.009	0.0143
2ME + polyether <sup>c</sup>	0.0712	0.032	0.0025	0.0028	0.0045	0.0372
alkoxyethanol + propylamine <sup>c</sup>	0.0362	0.0234	0.0048	0.0088	0.032	0.0902

<sup>a</sup>Calculated as  $1/N_s \sum \sigma_r(u)$ ,  $N_s$ , number of systems;<sup>b</sup>For symbols, see table 1;<sup>c</sup> $T = 298.15$  K;<sup>d</sup> $T = 303.15$  K.Table 6. Molecular interaction parameter,  $\chi$  and deviations from the ideal mixing of intermolecular free length,  $\Delta L_f$ , for hydroxyether + organic solvent mixtures at 298.15 K and equimolar composition.

System <sup>a</sup>	$\chi = (u_{\text{exp}}/u_{\text{id}})^2 - 1$	$\Delta L_f/10^{-11}$ m
2EE + C <sub>8</sub>	$-9.0 \times 10^{-3}$	0.119
2PE + C <sub>8</sub>	$1.3 \times 10^{-3}$	0.076
2BE + C <sub>8</sub>	$2.3 \times 10^{-3}$	0.063
2ME + 4O4	$7.2 \times 10^{-3}$	-0.013
2EE + 4O4	$8.2 \times 10^{-3}$	0.005
2BE + 4O4	$2.1 \times 10^{-2}$	-0.037
22MEE + 4O4	$3.9 \times 10^{-2}$	-0.025
22EEE + 4O4	$3.2 \times 10^{-2}$	-0.006
22BEE + 4O4	$3.8 \times 10^{-2}$	-0.028
222MEEE + 4O4	$5.9 \times 10^{-2}$	0.0001
222EEEE + 4O4	$5.4 \times 10^{-2}$	0.011
222BEEE + 4O4	$5.5 \times 10^{-2}$	-0.011
2ME + 1O2O1	$4.3 \times 10^{-2}$	0.10
2ME + 1O2O2O1	$9.7 \times 10^{-3}$	-0.090
2ME + 1O2O2O2O1	$6.3 \times 10^{-3}$	-0.074
2ME + 2O2O2O2	$1.3 \times 10^{-2}$	-0.112
2ME + 4O2O2O4	$2.8 \times 10^{-3}$	-0.039
2ME + propylamine	$9.3 \times 10^{-2}$	-0.399
22MEE + propylamine	0.124	-0.322
22EEE + propylamine	0.10	-0.359
22BEE + propylamine	0.1354	-0.265
222MEEE + propylamine	0.148	-0.292

<sup>a</sup>For symbols, see table 1.

#### 4. Discussion

We note that CFT, Nomoto's and Junjie's equations provide the same average results on speeds of sound (tables 4 and 5), magnitude represented quite accurately by these three models. The poorer predictions are obtained when applying the Junjie's equation to propylamine systems, probably due to the existence of strong interactions between

unlike molecules in such mixtures. The following evidence supports this conclusion. (i) Very negative  $V^E$  values, which are of the same order than those of 1-alkanol + amine systems, characterized by strong hydrogen bonds of the O–H–N type [46,47]. For example, at 298.15 K and equimolar composition,  $V^E$  (methanol + butylamine) =  $-1.677$  [48];  $V^E$ (1-propanol + propylamine) =  $-1.315$  [49];  $V^E$ (1-propanol + triethylamine) =  $-1.997$  [50], all values in  $\text{cm}^3 \text{mol}^{-1}$ . (ii) Negative  $\Delta L_f$  values and  $u$  values which are higher than those of the other mixtures investigated in the present work. This is in agreement with the fact that  $u$  increases with the decrease of  $L_f$  and vice versa [51,52]. (iii) Positive  $\chi$  values [44]. The discrepancies between experimental and calculated speeds of sound may be explained if one takes into account that the Junjie's equation is based on the ideal mixing concept. This also may explain results from Van Dael's equation, where, in addition, it is assumed that  $V_1 = V_2$ . Note the large deviations encountered for those systems with components of very different size, e.g. 2-methoxyethanol + 5,8,11-trioxapentadecane or 2-{2-(2-methoxyethoxy)ethoxy}ethanol + propylamine (table 4).

The good  $u$  predictions obtained using Nomoto's equation remark the validity of Rao's assumption on additivity of molar sound velocity contributions (Rao's constant) from atoms, atom groups and chemical bonds of the constituent molecules (see further) [53].

On the other hand, results from CFT support the generalization of equation (10) for liquid mixtures ( $S = \sum x_i S_i$  and  $B = \sum x_i B_i$ ). Moreover, it is also a test of equation (9). The validity of this expression to calculate the molecular radius has been discussed elsewhere [41]. We note that slightly better  $u$  predictions from this model are obtained for the systems 2-methoxyethanol + polyether, or hydroxyether + propylamine (tables 4 and 5). That is, for those mixtures where rather strong interactions between unlike molecules are expected. In the case of 2-methoxyethanol + polyether systems, interactions can be considered to be of dipole–dipole type as the decrease of  $H^E$  with the number of oxygen atoms in the oxaalkane suggests. At equimolar composition and 298.15 K,  $H^E$  (2-ethoxyethanol + 2,5-dioxahexane) =  $338 \text{ J mol}^{-1}$  [54] <  $H^E$  (2-ethoxyethanol + dibutylether) =  $1008 \text{ J mol}^{-1}$  [55] and  $H^E$  (2-butoxyethanol + 2,5,8-trioxanonane) =  $592 \text{ J mol}^{-1}$  <  $H^E$  (2-butoxyethanol + dibutylether) =  $680 \text{ J mol}^{-1}$  [56]. For ester (methylacetate or ethylacetate) + hexane systems, characterized by large positive  $H^E$ ,  $V^E$  and  $\Delta k_s$  values, CFT yields deviations for  $u$  which are of 3.3% (methylacetate) and 2.1% (ethylacetate) [42]. This maybe explained taking into account the destruction of the dipolar order in the ester molecules by adding nonpolar hexane molecules [42]. It seems that the model provides better results for ordered systems.

Free length theory yields a larger average  $\sigma_r(u)$  value than those from CFT, Nomoto's or Junjie's equations (table 5). This might be explained in terms of two important shortcomings of the model: association and shape or size effects [57,58]. For example, it should be kept in mind that equation (3) is valid for spherical molecules only. So, we note that the largest  $\sigma_r(u)$  value is encountered for the system containing 5,8,11-trioxapentadecane, the longest molecule considered in this work (table 4). Shape effects could also explain the observed increase in  $\sigma_r(u)$

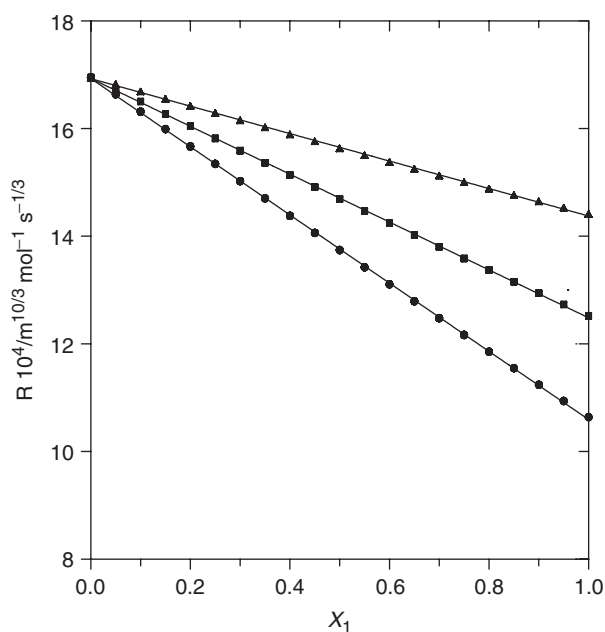


Figure 1. Molar sound velocity,  $R$ , at 298.15 K for 2-alkoxyethanol(1)+octane(2) mixtures. Points, experimental results using data from the literature [64]: (●), 2EE; (■), 2PE; (▲), 2BE. Solid lines, linear regressions.

when replacing, in mixtures with dibutylether, the 2-alkoxyethanol or 2-(2-alkoxyethoxy)ethanol by a hydroxyether with three etheric atoms. The good results obtained for the systems 2-butoxyethanol+octane, or +dibutylether, or 2-(2-methoxyethoxy)ethanol+dibutylether, formed by compounds of similar size are remarkable. On the other hand, the rather large  $\sigma_r(u)$  values for mixtures such as 2-methoxyethanol+2,5-dioxahexane, or +propylamine maybe due to association effects (see above).

Finally, we note that equation (12) gives the poorer  $u$  predictions, as it depends too directly on  $V_0$ .

It is known that the molar sound velocity in binary liquid mixtures is a linearly dependent magnitude on the molar fractions of the component liquids ( $R=x_1R_1+x_2R_2$ ) in the case there is no association, or in the case that the degree of association does not change with concentration, as long as the density of the component liquids does not differ largely [28,59,60]. Deviations from this behavior are also encountered for mixtures with a component containing halogen atom [42,61]. For the investigated mixtures, the Rao's constant varies linearly with the concentration (figures 1–6), and this indicates the absence of complex formation [59,60]. Such conclusion is also supported by the linear dependence of the Wada's constant with mole fraction (figures 7 and 8). This newly remarks the importance of dipole-dipole interactions in the studied systems. Here it is pertinent to remark that

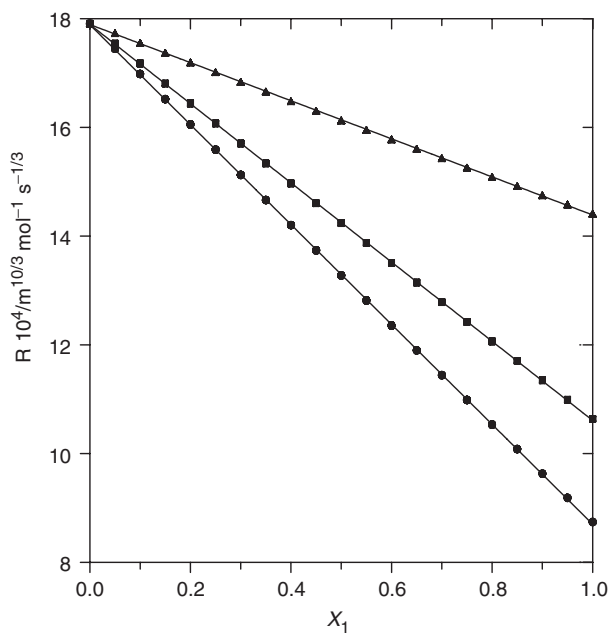


Figure 2. Molar sound velocity,  $R$ , at 298.15 K for 2-alkoxyethanol(1)+dibutylether(2) mixtures. Points, experimental results using data from the literature [23]: (●), 2ME; (■), 2EE; (▲), 2BE. Solid lines, linear regressions.

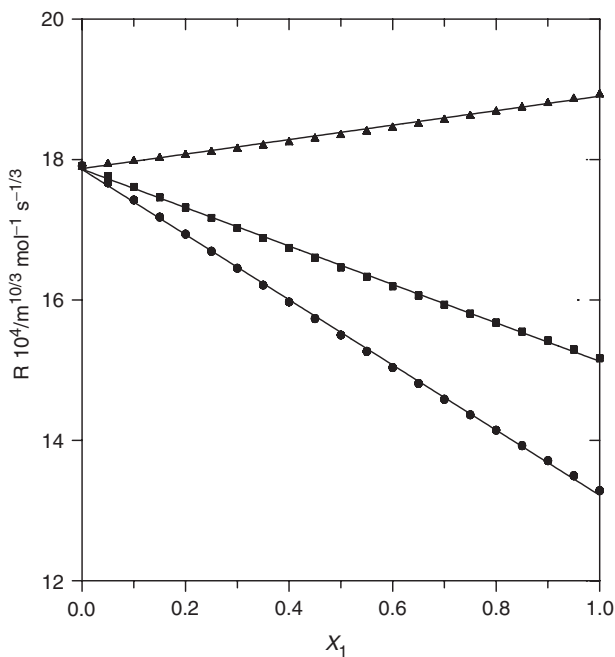


Figure 3. Molar sound velocity,  $R$ , at 298.15 K for 2-(2-alkoxyethoxy)ethanol(1)+dibutylether(2) mixtures. Points, experimental results using data from the literature [24]: (●), 22ME; (■), 22EE; (▲), 22BE. Solid lines, linear regressions.

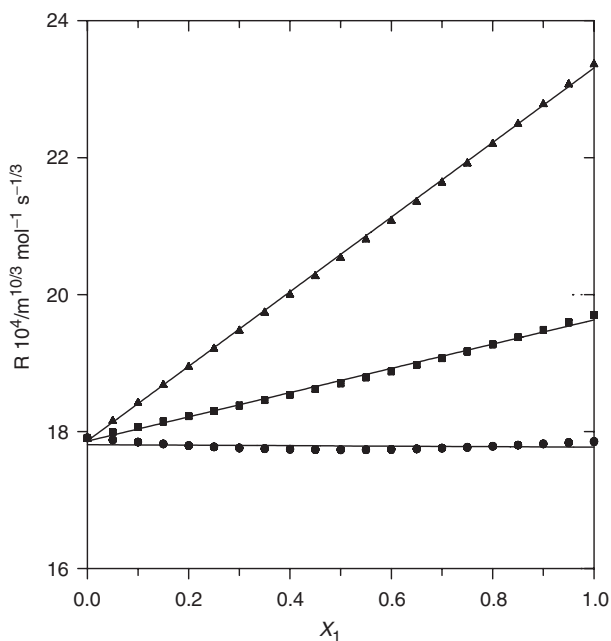


Figure 4. Molar sound velocity,  $R$ , at 298.15 K for 2-(2-(2-alkoxyethoxy)ethoxy)ethanol(1) + dibutylether(2) mixtures. Points, experimental results using data from the literature [65,66]: (●), 222MEEE; (■), 222EEEE; (▲), 222BEEE. Solid lines, linear regressions.

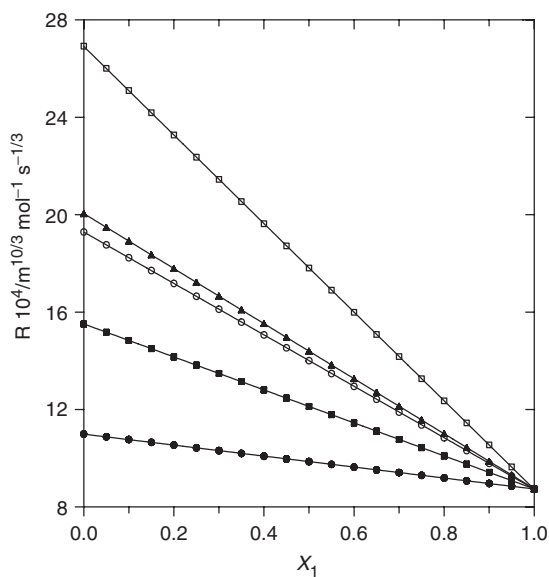


Figure 5. Molar sound velocity,  $R$ , at 298.15 K for 2-methoxyethanol(1) + oxaalkane(2) mixtures. Points, experimental results using data from the literature [67, 68]: (●), 2,5-dioxahehexane; (■), 2,5,8-trioxaundecane; (▲), 2,5,8,11-tetraoxadecane; (●), 3,6,9-trioxaundecane; (□), 5,8,11-trioxapentadecane. Solid lines, linear regressions.

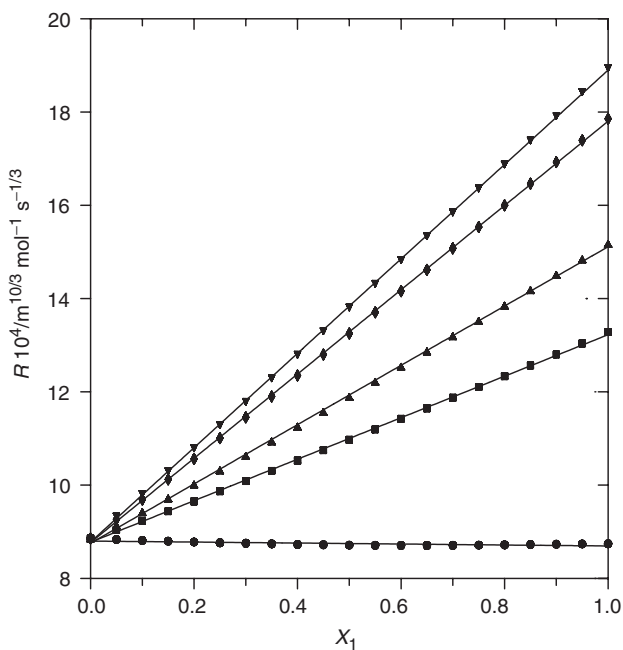


Figure 6. Molar sound velocity,  $R$ , at 298.15 K for hydroxyether(1) + propylamine(2) mixtures. Points, experimental results using data from the literature [69,70]: (●), 2ME; (■), 22MEE; (▲), 22EE; (▼), 22BE; (◆), 222MEEE. Solid lines, linear regressions.

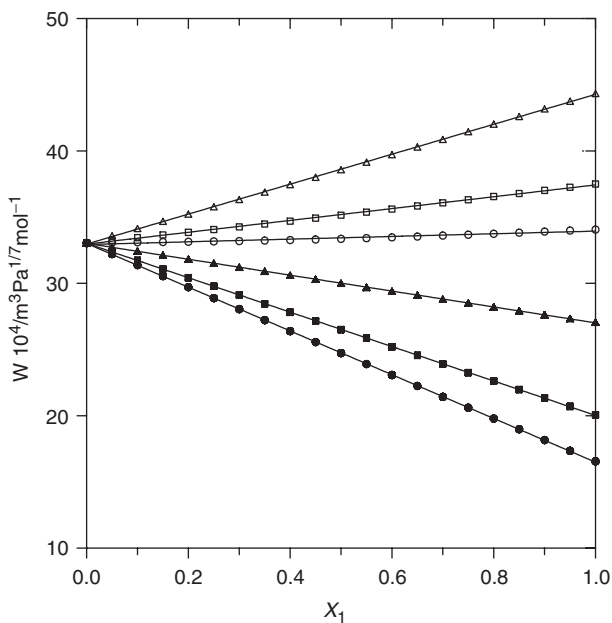


Figure 7. Molecular compressibility,  $W$ , at 298.15 K for hydroxyether(1) + dibutylether(2) mixtures. Points, experimental results using data from the literature [23,65,66]: (●), 2ME; (■), 2EE; (▲), 2BE; (●), 222MEEE; (□), 222ESEE; (Δ), 222BEEE. Solid lines, linear regressions.

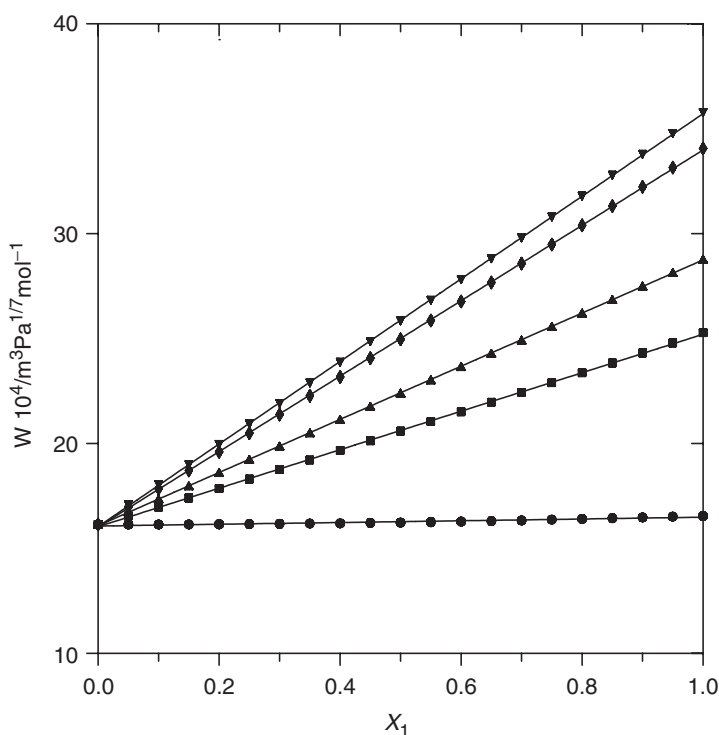


Figure 8. Molecular compressibility,  $W$ , at 298.15 K for hydroxyether(1) + propylamine(2) mixtures. Points, experimental results using data from the literature [69,70]: (●), 2ME; (■), 22MEE; (▲), 22EE; (▼), 22BE; (◆), 22MEEE. Solid lines, linear regressions.

the Rao's and Wada's constant have been theoretically developed on the basis of an interaction potential of the Lennard-Jones type [62,63].

The  $\chi$  parameter (or a parameter defined merely as  $(u_{\text{exp}}/u_{\text{id}})^2$ ) is widely used to estimate the non-ideality of a system, as systems with stronger deviations from the ideal behavior are characterized by high  $\chi$  values. For example, for mixtures involving 2-pyrrolidone,  $\chi$  (methanol)  $\approx 0.8$  and  $\chi$  (ethanol)  $\approx 0.35$  [39]. The low  $\chi$  values listed in table 6 indicate that the investigated mixtures are, in terms of the speed of sound, close to the ideal behavior. The good  $u$  predictions obtained using the Junjie's equation support such conclusion. The concentration dependence of  $\chi$  is shown, for a few examples, in figures 9 and 10. For propylamine mixtures, the curves become shifted to lower mole fractions of hydroxyether when its size increases. That is, interactions between unlike molecules are more probable in that region. In the case of dibutylether systems, the corresponding curves are skewed towards higher mole fractions of the alkoxyethanol. This reveals that the oxaalkane is an active breaker of the hydroxyether structure at low concentrations of this component. Finally, it should be noted that for, a given solvent, propylamine or dibutylether,  $\chi$  increases by increasing the number of oxyethylene groups in the hydroxyether.

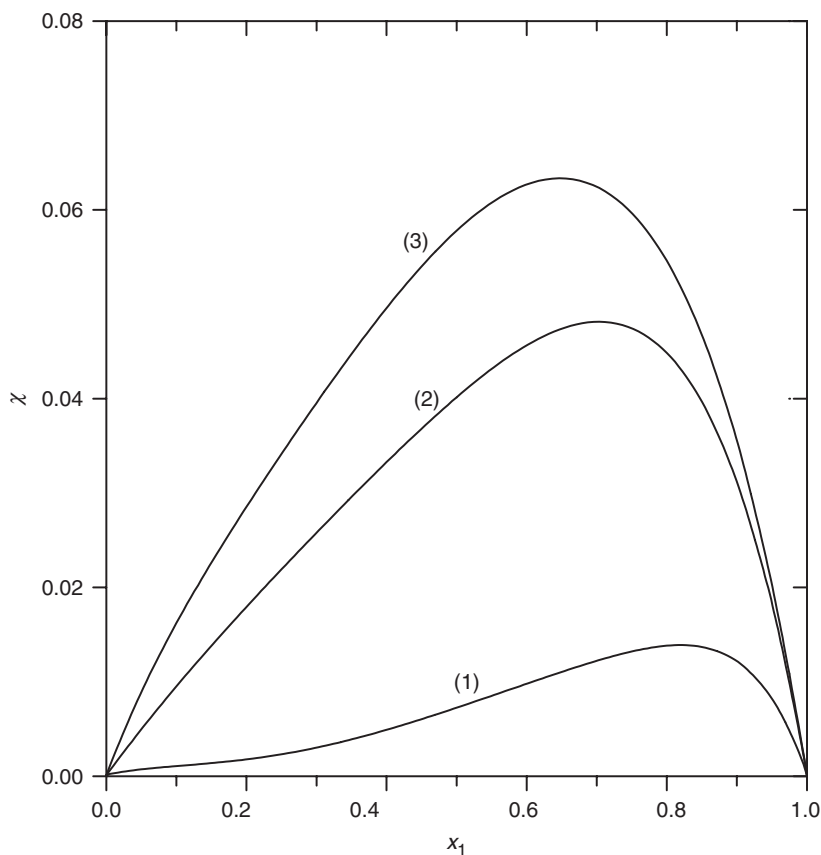


Figure 9. Interaction molecular parameter,  $\chi$ , at 298.15 K for hydroxyether(1) + dibutylether(2) mixtures: (1), 2ME; (2), 22MEE; (3), 222MEEE.

## 5. Conclusions

Collision factor theory, Nomoto's and Junjie's equations provide similar deviations between experimental and calculated  $u$ , which is represented quite accurately by these three models. Poorer predictions are obtained when applying the Junjie's equation to propylamine systems, probably due to the existence of strong interactions between unlike molecules in such mixtures. Slightly better  $u$  predictions from CFT are obtained for the systems 2-methoxyethanol + polyether, or hydroxyether + propylamine. The good  $u$  predictions obtained using Nomoto's equation remark the validity of Rao's assumption on additivity of molar sound velocity contributions from atoms, atom groups and chemical bonds of the constituent molecules. The larger discrepancies between experimental and calculated  $u$  from FLT are explained in terms of association and shape or size effects. Interactions in the investigated mixtures are of dipolar type. This is supported by the linear dependence on the molar fractions of the component liquids of the Rao's and Wada's constants.



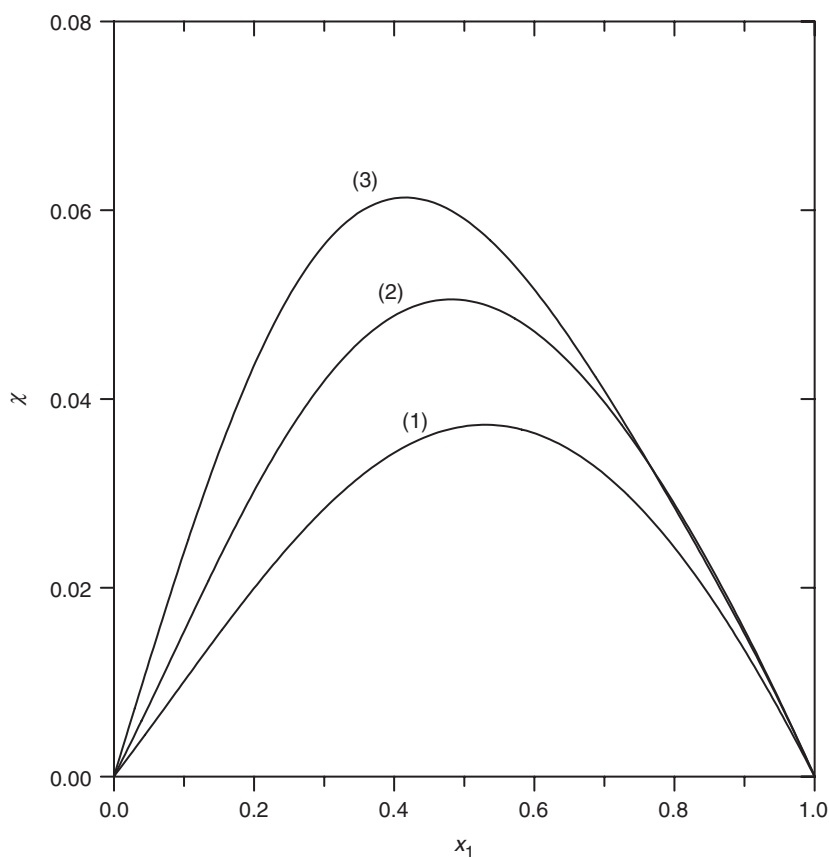


Figure 10. Interaction molecular parameter,  $\chi$ , at 298.15 K for hydroxyether(1) + propylamine(2) mixtures: (1), 2ME; (2), 22MEE; (3), 222MEEE.

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